



PATENT

Docket No.: HOE 92/F 294

Patent Application
Commissioner of Patents and Trademarks
Washington, D.C. 20231

10965 S. PRO
08/120105
09/10/93

NEW APPLICATION TRANSMITTAL

Transmitted herewith for filing is the patent application of

Inventors: Andreas Winter, Walter Spaleck, and Bernd Bachmann

For: Polyolefin Molding Composition Having a Broad Melting
Range, Process for its Preparation, and its Use

1. Type of Application

This new application is for a(n)

- ☒ Original
- ☐ Design
- ☐ Plant
- ☐ Divisional
- ☐ Continuation
- ☐ Continuation-in-part (CIP)

2. Benefit of Prior U.S. Application(s) (35 USC 120)

- ☐ The new application being transmitted claims the benefit of prior U.S. application(s) and enclosed are ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED.

CERTIFICATION UNDER 37 CFR 1.10

I hereby certify that this New Application Transmittal and the documents referred to as enclosed therein are being deposited with the United States Postal Service on September 10, 1993 in an envelope as "Express Mail Post Office to Addressee" Mailing Label Number TB21627099XUS addressed to: Commissioner of Patents and Trademarks, Washington, D.C. 20231.

Linda J. Scheurle

3. Papers Enclosed Which Are Required For Filing Date Under 37 CFR 1.53(b) (Regular) or 37 CFR 1.153 (Design) Application

29 Pages of specification

6 Pages of claims

1 Pages of Abstract

0 Sheets of drawing

☐ formal

☐ informal

4. Additional Papers Enclosed

☒ Preliminary Amendment

☐ Information Disclosure Statement (37 CFR 1.98)

☐ Form PTO-1449

☐ Citations

☐ Declaration of Biological Deposit

☐ Submission of "Sequence Listing", computer readable copy and/or amendment pertaining thereto for biotechnology invention containing nucleotide and/or amino acid sequence

☐ Authorization of Attorney(s) to Accept and Follow Instructions from Representative

☐ Special Comments

☐ Other

5. Declaration or Oath

☒ Enclosed
executed by

☒ inventors

☐ legal representative of inventor(s) (37 CFR 1.42 or 1.43)

☐ joint inventor or person showing a proprietary interest on behalf of inventor who refused to sign or cannot be reached

☐ this is the petition required by 37 CFR 1.47 and the statement required by 37 CFR 1.47 is also attached

☐ Not enclosed

☐ Application is made by a person authorized under 37 CFR 1.41(c) on behalf of all the above named inventor(s)

☐ showing that the filing is authorized

6. Inventorship Statement

The inventorship for all the claims in this application are:

☒ the same

or

☐ not the same. An explanation, including the ownership of the various claims at the time the last claimed invention was made,

☐ is submitted.

☐ will be submitted.

7. Language

☒ English

☐ non-English

☐ the attached translation is a verified translation. 37 CFR 1.52(d).

8. Assignment

☒ An assignment of the invention to Hoechst Aktiengesellschaft

☒ is attached

☒ A separate "COVER SHEET FOR ASSIGNMENT (DOCUMENT) ACCOMPANYING NEW PATENT APPLICATION" or

☐ FORM PTO 1595

is also attached

☐ will follow

9. Certified Copy

Certified copy(ies) of application(s)

Germany	P 42 30 530.6	September 12, 1992
(country)	(appln. no.)	(filed)
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(country)	(appln. no.)	(filed)

from which priority is claimed

☒ is (are) attached

☐ will follow

10. Fee Calculation (37 CFR 1.16)

☒ A. Regular Application

CLAIMS AS FILED			
Number Filed	Number Extra	Rate	Basic Fee 37 CFR 1.16(a) \$710.00
Total Claims (37 CFR 1.16(c)) 11 – 20 =	0 X	\$22.00	\$0.00
Independent Claims (37 CFR 1.16(b)) 5 – 3 =	2 X	\$74.00	\$148.00
Multiple Dependent Claims, if any (37 CFR 1.16(d)) 0 =	0 X	\$230.00	\$0.00
<input type="checkbox"/> Amendment cancelling extra claims enclosed <input type="checkbox"/> Amendment deleting multiple-dependencies enclosed <input type="checkbox"/> Fee for extra claims is not being paid at this time			
Filing Fee Calculation:			\$858.00

☐ B. Design Application
 (\$290.00 – 37 CFR 1.16(f))
 Filing Fee Calculation: \$ _____

☐ C. Plant Application
 (\$460.00 – 37 CFR 1.16(g))
 Filing Fee Calculation: \$ _____

11. Small Entity Statement(s)

☐ Verified Statement(s) that this is a filing by a small
 entity under 37 CFR 1.9 and 1.27 is (are) attached
 Filing Fee Calculation (50% of A, B or C above): \$ _____

12. Request for International-Type Search (37 CFR 1.104(d))

- ☐ Please prepare an international-type search report for this application at the time when national examination on the merits takes place.

13. Fee Payment Being Made At This Time

- ☐ Not Enclosed
☐ No filing fee is to be paid at this time.

☒ Enclosed

☒ basic filing fee \$ 858.00

☒ recording assignment \$ 40.00
(\$40.00; 37 CFR 1.21(h))

☐ petition fee for filing by other than
all the inventors or person on behalf
of the inventor where inventor refused
to sign or cannot be reached.
(\$130.00; 37 CFR 1.47 and 1.17(h)) \$ _____

☐ for processing an application with a
specification in a non-English language.
(\$130.00; 37 CFR 1.52(d) and 1.17(k)) \$ _____

☐ processing and retention fee
(\$130.00; 37 CFR 1.53(d) and 1.21(l)) \$ _____

☐ fee for international-type search report
(\$40.00; 37 CFR 1.21(e)) \$ _____

Total fees enclosed \$ 898.00

14. Method of Payment of Fees

☐ Check in the amount of \$ _____

☒ Charge Account No. 08-2453 in the amount of \$ 898.00. A duplicate of this transmittal is attached.

15. Authorization to Charge Additional Fees

- ☒ The Commissioner is hereby authorized to charge the following additional fees by this paper and during the entire pendency of this application to Account No. 08-2453.
 - ☒ 37 CFR 1.16(a), (f) or (g) (filing fees)
 - ☒ 37 CFR 1.16(b), (c) and (d) (presentation of extra claims)
 - ☐ 37 CFR 1.16(e) (surcharge for filing the basic filing fee and/or declaration on a date later than the filing date of the application)
 - ☐ 37 CFR 1.17 (application processing fees)
 - ☐ 37 CFR 1.18 (issue fee at or before mailing of Notice of Allowance, pursuant to 37 CFR 1.311(b))

16. Instructions As To Overpayment

- ☒ credit Account No. 08-2453
- ☐ refund



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☒ Incorporation by reference of added pages

☐ Plus Added Pages For New Application Transmittal Where Benefit Of Prior U.S. Application(s) Claimed

Number of pages added _____

☒ Plus Added Pages For Pages Referred To In Item 4 Above

Number of pages added 6

☒ Plus "Assignment Cover Letter Accompanying New Application"

Number of pages added 5

☐ Statement Where No Further Pages Added

☐ This transmittal ends with this page.

08/120105



09/10/93

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re application of: Winter et al.

Serial No.:

Group No.:

Filed:

Examiner:

For: POLYOLEFIN MOLDING COMPOSITIONS
HAVING A BROAD MELTING RANGE,
PROCESS FOR ITS PRODUCTION AND
ITS USE

Docket: HOE 92/F 294

Commissioner of Patents and Trademarks
Washington D.C. 20231

AMENDMENT ACCOMPANYING NEW APPLICATION TRANSMITTAL

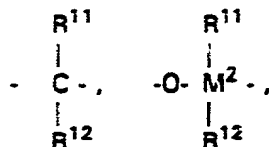
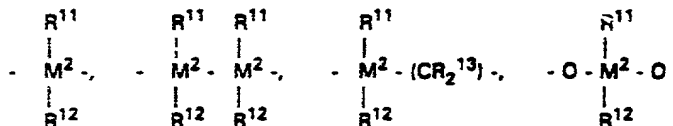
Sir:

Applicants respectfully request consideration of the present amendment which is intended to correct errors of a typographical nature, place the claims in a form which conforms to U.S. patent practice and add new claims which find their support in the original specification.

IN THE SPECIFICATION:

On page 6, delete line 14 and the following formulas and substitute therefor:

R⁵ is



On page 23, line 30, delete "ZrCl₃" and substitute therefor -- ZrCl₂ --.

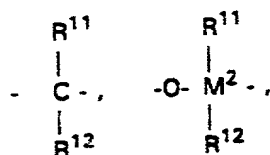
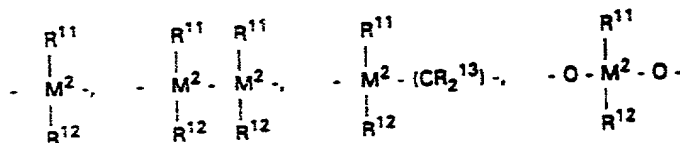
IN THE CLAIMS:

In claim 2, page 30, line 9, delete "A" and insert therefor -- The --.

In claim 6, page 31, line 2, delete "5" and substitute therefor -- 12 --.

In claim 7, page 33, delete line 30 and the following formulas and substitute therefor:

R⁵ is



3. (Amended) [A] The polyolefin molding composition as claimed in claim 1, which additionally contains one or more additives selected from the group consisting of nucleating agents, stabilizers, antioxidants, UV absorbers, light stabilizers, metal deactivators, free-radical scavengers, fillers and reinforcing agents, compatibilizers, plasticizers, lubricants, emulsifiers, pigments, optical brighteners, flameproofing agents, antistatics and blowing agents.

Delete claims 4, 5, 9 and 10.

Add new claims 11 - 15:

11. A process for the preparation of a polyolefin molding composition having a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C and the width determined at quarter peak height is greater than 15°C, wherein such process comprises mixing at least two polyolefins of different melting points, where the melting points of at least two of the polyolefins must differ by at least 5°C, the viscosity indices are greater than $VI = 10 \text{ cm}^3/\text{g}$ and the molecular weights M_w are greater than 5000 g/mol.
12. A process for the preparation of a polyolefin molding composition having a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C and the width determined at quarter peak height is greater than 15°C, wherein such process comprises direct polymerization or copolymerization of at least two polyolefins of different melting point, where the melting points must differ by at least 5°C.
13. A method of using a molding composition for the production of moldings, wherein the molding composition comprises a polyolefin molding composition

having a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C and the width determined at quarter peak height is greater than 15°C.

14. A molding comprising a polyolefin molding composition having a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C and the width determined at quarter peak height is greater than 15°C.
15. The process as claimed in claim 6, wherein the metallocenes are selected from the group consisting of $\text{rac-Me}_2\text{Si}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-Me}_2\text{Si}(\text{indenyl})_2\text{HfCl}_2$, $\text{phenyl(methyl)Si}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$, $\text{Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$, $\text{Me}_2\text{Si}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$, $\text{Me}_2\text{Si}(\text{indenyl})_2\text{HfCl}_2$, $\text{phenyl(methyl)silyl}(\text{indenyl})_2\text{HfCl}_2$, $\text{rac-ethylene}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-ethylidene}(2\text{-methyl-4,6-diisopropyl-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-Me}_2\text{Si}(2\text{-methyl-4,5-benzoindenyl})_2\text{ZrCl}_2$, $\text{dimethylmethylene}(9\text{-fluorenyl})(\text{cyclopentadienyl})\text{ZrCl}_2$, $\text{phenyl(methyl)methylene}(9\text{-fluorenyl})(\text{cyclopentadienyl})\text{ZrCl}_2$, $\text{rac-phenyl(methyl)silyl}(2\text{-methyl-4,6-diisopropyl-1-indenyl})_2\text{ZrCl}_2$, $\text{Ph(Me)Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$, $\text{rac-Me}_2\text{Si}(2,5,6\text{-trimethyl-1-indenyl})_2\text{ZrCl}_2$, rac-

Me₂Si(4.5-benzo-1-indenyl)₂ZrCl₂ and rac-Me₂Si(4-phenyl-1-indenyl)₂ZrCl₂.

REMARKS

The amendment to the specification corrects certain typographical errors. Support for the amendment on page 6, line 14, of the specification is found on page 7, lines 1 - 15, of the priority document.

In the claims, the amendment to claim 2 is non-substantive and the amendment to claim 6 is necessary in view of the substitution of new claim 12 for claim 5 which has been deleted. The amendment to claim 7 corrects a typographical error and support is found on page 31, lines 1 - 15, of the priority document. Claim 3 has been amended to clarify that the composition of claim 1 may contain one or more of the recited additives.

Claims 4, 5, 9 and 10, which were originally written in dependent form, have been deleted and rewritten as independent claims 11, 12, 13 and 14, respectively.

New claim 15 recites the specific metallocene compounds of the working examples.

No new matter has been added by the amendment made to the claims.

CONCLUSION

It is respectfully requested that the claims of the referenced application be amended in the manner set forth in this preliminary amendment. The preliminary amendment requires a fee of \$148.00 since two (2) independent claims in excess of three (3) have been filed, to date, in connection with this application. However, the total number of claims does not exceed 20. Please charge Deposit Account #08-2453 to satisfy the charge for the two (2) independent claims in excess of three (3).

It is submitted that the application is in condition for allowance, which action is respectfully requested.



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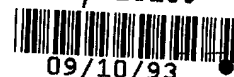
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Description

Polyolefin molding composition having a broad melting range, process for its preparation, and its use

- 5 As a rule, metallocene/aluminoxane catalyst systems allow the preparation of polyolefins or polyolefin copolymers having a sharp melting point. These products are highly suitable, for example, for thin-wall injection molding or precision injection molding, giving very short cycle
- 10 times per injection-molded part.

- By contrast, many applications, for example thermoforming, blow molding, extrusion, injection stretch blow molding and certain film applications are unsuitable for a polyolefin having such a sharp melting and crystallization range.
- 15

- In thermoforming, a product of this type leads to process problems and, for example, moldings having uneven wall thicknesses. In film applications, heat-sealing or stretching, for example, is difficult with a product
- 20 having a sharp melting point. Such applications require a polyolefin having a broad melting range.

- The object was to find a process which enables the preparation of polyolefin molding compositions having a broad melting range. The object has been achieved by
- 25 polymerization or copolymerization of the olefin or olefins by means of at least two different metallocenes.

- At a certain polymerization temperature, a polyolefin having a certain melting point is formed due to the stereospecificity of each type of metallocene catalyst.
- 30 Surprisingly, it has now been found that a mixture of at least two metallocenes each of which gives polyolefins of very different melting points give a polyolefin mixture

which does not, as expected, have a mixed melting point or a melting point below the melting point of the lower-melting component, but instead gives a polymer product which has two melting points. The melting range determined by means of the DSC ("differential scanning calorimeter") spectrum is, in direct comparison with the separate polymers, significantly broadened or even bimodal, and the product has the above-discussed advantages on conversion into moldings.

10 In addition it has been found that the mixing of polyolefins having different melting points, for example by extrusion, likewise gives a product which has a broad bimodal or multimodal melting range.

The invention thus relates to the preparation of a polyolefin molding composition having the following properties:

The molding composition has a broad, bimodal or multimodal melting range in the DSC spectrum. The melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C, and the width determined at the quarter peak height is greater than 15°C. In addition, the half-intensity width of the crystallization peak is greater than 4°C and the width of the crystallization peak determined at the quarter peak height is greater than 6°C.

Fractional crystallization or extraction with hydrocarbons allows the molding composition to be separated into its components, and the resultant polyolefin components have relatively sharp melting and crystallization peaks.

In addition to the polyolefin, the molding composition according to the invention may also contain conventional additives, for example nucleating agents, stabilizers, antioxidants, UV absorbers, light stabilizers, metal deactivators, free-radical scavengers, fillers and

reinforcing agents, compatibilizers, plasticizers, lubricants, emulsifiers, pigments, optical brighteners, flameproofing agents, antistatics and blowing agents.

This novel polyolefin molding composition is prepared

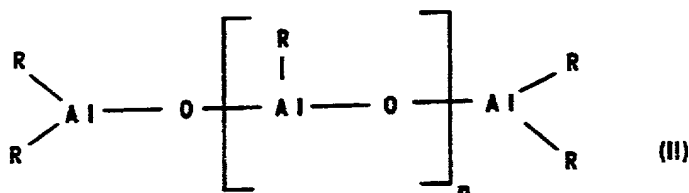
- 5 a) by mixing at least two, preferably two or three, polyolefins of different melting points. The melting points of at least two of the polyolefins must differ by at least 5°C. There are no restrictions on the mixing ratio of the polyolefins nor on the molecular weight dispersity. The viscosity index should be greater than $VI = 10 \text{ cm}^3/\text{g}$, and the molecular weight M_v should be greater than 5000 g/mol. The polymers can be mixed by one of the methods conventional in plastics processing. One possibility is sintering in a high-speed mixer if the polymers to be mixed are pulverulent, and another possibility is the use of an extruder having mixing and compounding elements on the screw, or the use of a compounder as used in the rubber industry, or
- 10
- 15
- 20 b) by direct polymerization of at least two, preferably two or three, polyolefins of different melting point. The melting points of at least two of the polyolefins must differ by at least 5°C. There are no restrictions on the mixing ratio of the polyolefins prepared in the polymerization.
- 25

This direct polymerization of the polyolefin molding composition according to the invention is carried out by polymerization or copolymerization of olefins of the formula $R^aCH=CHR^b$, in which R^a and R^b are identical or different and are a hydrogen atom or an alkyl radical having 1 to 14 carbon atoms, or R^a and R^b , together with the atoms connecting them, can form a ring, at a temperature of from -60 to 200°C, a pressure of from 0.5 to 100 bar, in solution, in suspension or in the gas phase,

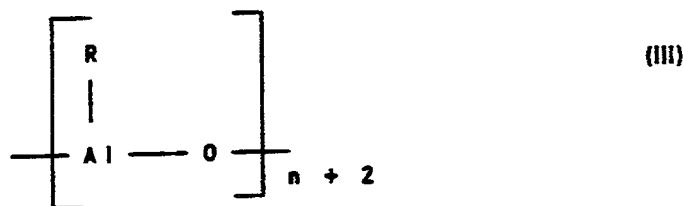
30

35 in the presence of a catalyst which comprises at least

two transition-metal components (metallocenes) and an aluminoxane of the formula II

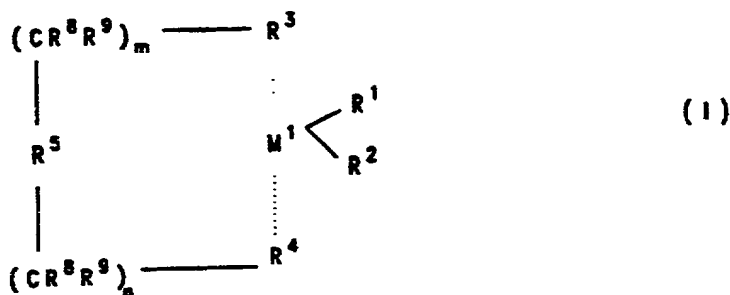


for the linear type and/or of the formula III



for the cyclic type, where, in the formulae II and III, the radicals R may be identical or different and are a C₁-C₆-alkyl group, a C₁-C₆-fluoroalkyl group, a C₆-C₁₈-aryl group, a C₆-C₁₈-fluoroaryl group or hydrogen, and n is an integer from 0 to 50, and the aluminoxane component may additionally contain a compound of the formula AlR₃,

where the transition-metal component used comprises at least two metallocenes of the formula I:



in which

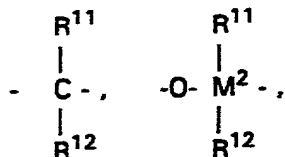
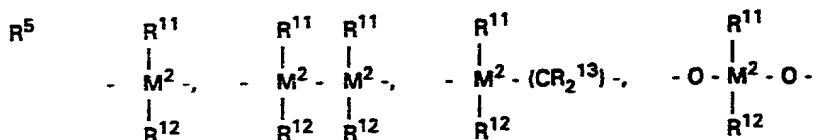
M¹ is Zr, Hf or Ti,

R¹ and R² are identical or different and are a hydrogen atom, a C₁-C₁₀-alkyl group, a C₁-C₁₀-alkoxy group, a C₆-C₁₀-aryl group, a C₆-C₁₀-aryloxy group, a C₂-C₁₀-alkenyl group, a C₇-C₄₀-arylalkyl group, a

C₇-C₄₀-alkylaryl group, a C₈-C₄₀-arylalkenyl group or a halogen atom,

R³ and R⁴ are identical or different and are a monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radical which, together with the metal atom M¹, can form a sandwich structure,

R⁵ is



=BR¹¹, =AlR¹¹, -Ge-, -Sn-, -O-, -S-, =SO, =SO₂, =NR¹¹, =CO, =PR¹¹ or =P(O)R¹¹,

10 where

R¹¹, R¹² and R¹³ are identical or different and are a hydrogen atom, a halogen atom, a C₁-C₁₀-alkyl group, a C₁-C₁₀-fluoroalkyl group, a C₆-C₁₀-aryl group, a C₆-C₁₀-fluoroaryl group, a C₁-C₁₀-alkoxy group, a C₂-C₁₀-alkenyl group, a C₇-C₄₀-arylalkyl group, a C₈-C₄₀-arylalkenyl group or a C₇-C₄₀-alkylaryl group, or R¹¹ and R¹² or R¹¹ and R¹³, in each case together with the atoms connecting them, form a ring, and M² is silicon, germanium or tin,

20 R⁸ and R⁹ are identical or different and are as defined for R¹¹,

m and n are identical or different and are zero, 1 or 2, where m plus n is zero, 1 or 2.

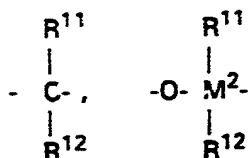
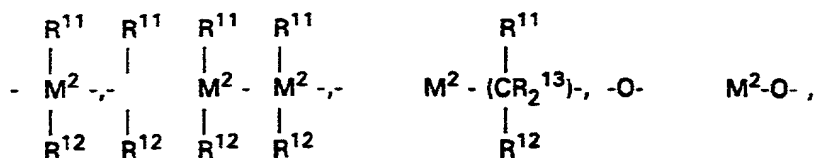
Alkyl is straight-chain or branched alkyl. Halogen (halogenated) denotes fluorine, chlorine, bromine or iodine, preferably fluorine or chlorine.

M¹ is Zr, Hf or Ti, preferably Zr or Hf.

R¹ and R² are identical or different and are a hydrogen atom, a C₁-C₁₀-, preferably C₁-C₃-alkyl group, a C₁-C₁₀-, preferably C₁-C₃-alkoxy group, a C₆-C₁₀-, preferably C₆-C₈-aryl group, a C₆-C₁₀-, preferably C₆-C₈-aryloxy group, a C₂-C₁₀-, preferably C₂-C₄-alkenyl group, a C₇-C₄₀-, preferably C₇-C₁₀-arylalkyl group, a C₇-C₄₀-, preferably C₇-C₁₂-alkylaryl group, a C₈-C₄₀-, preferably C₈-C₁₂-arylalkenyl group or a halogen atom, preferably chlorine.

10 R³ and R⁴ are identical or different monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radicals which, together with the metal atom M¹, can form a sandwich structure.

R⁵ is



15 =BR¹¹, =AlR¹¹, -Ge-, -Sn-, -O-, -S-, =SO, =SO₂, =NR¹¹, =CO, =PR¹¹ or =P(O)R¹¹, where R¹¹, R¹² and R¹³ are identical or different and are a hydrogen atom, a halogen atom, a C₁-C₁₀-, preferably C₁-C₄-alkyl group, in particular a methyl group, a C₁-C₁₀-fluoroalkyl group, preferably a CF₃ group, a C₆-C₁₀-, preferably C₆-C₈-aryl group, a C₆-C₁₀-fluoroaryl group, preferably a pentafluorophenyl group, a C₁-C₁₀-, preferably C₁-C₄-alkoxy group, in particular a methoxy group, a C₂-C₁₀-, preferably C₂-C₄-alkenyl group, a C₇-C₄₀-, preferably C₇-C₁₀-arylalkyl group, a C₈-C₄₀-,

preferably C₈-C₁₂-arylalkenyl group or a C₇-C₄₀-, preferably C₇-C₁₂-alkylaryl group, or R¹¹ and R¹² or R¹¹ and R¹³, in each case together with the atoms connecting them, form a ring.

- 5 M² is silicon, germanium or tin, preferably silicon or germanium.

R⁵ is preferably =CR¹¹R¹², =SiR¹¹R¹², =GeR¹¹R¹², -O-, -S-, =SO, =PR¹¹ or =P(O)R¹¹.

- 10 R⁸ and R⁹ are identical or different and are as defined for R¹¹.

m and n are identical or different and are zero, 1 or 2, preferably zero or 1, where m plus n is zero, 1 or 2, preferably zero or 1.

- 15 Particularly preferred metallocenes are thus those in which M¹ is zirconium or hafnium, R¹ and R² are identical and are methyl or chlorine, R⁴ and R³ are indenyl, cyclopentadienyl or fluorenyl, where these ligands may carry additional substituents as defined for R¹¹, R¹² and R¹³, where the substituents may be different and, with the
20 atoms connecting them, may also form rings,

R⁵ is a



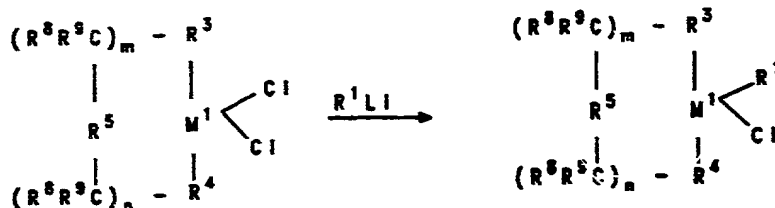
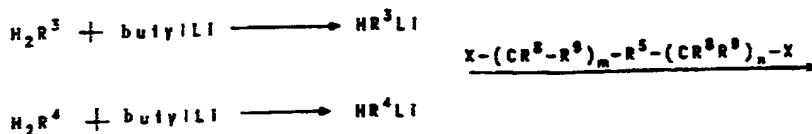
radical, and n plus m is zero or 1, in particular the compounds listed in the working examples.

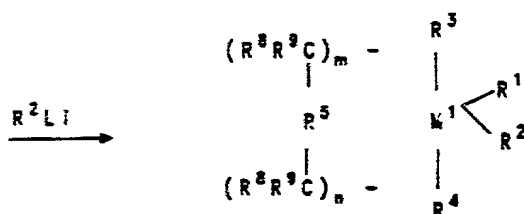
- 25 The chiral metallocenes are employed as a racemate for the preparation of highly isotactic polyolefins. However, the pure R or S form can also be used. These pure

stereoisomeric forms can be used to prepare an optically active polymer. However, the meso form of the metallocenes can be separated off, since the polymerization-active center (the metal atom) in these compounds is no longer chiral due to mirror symmetry at the central metal and a highly isotactic polymer therefore cannot be produced. If the meso form is not separated off, atactic polymer is formed in addition to isotactic polymer. For certain applications - soft moldings for example - this may be entirely desirable. Metallocenes having a formal C_s symmetry are suitable for the preparation of syndiotactic polyolefins.

The separation of the stereoisomers is known in principle.

15 In principle, the metallocenes I can be prepared by the following reaction scheme:





X = Cl, Br, I, O-Tosyl;

The preparation of the metallocene compounds is known.

The DSC measurements on the polyolefin composition according to the invention are preferably carried out at a heating or cooling rate of $\leq 20^\circ\text{C}/\text{min}$.

The choice of metallocenes for the polymerization of olefins to give polyolefins having a broad, bimodal or multimodal melting range can in each case take place by means of a test polymerization per metallocene.

- 10 In this test, the olefin is polymerized to the polyolefin and its melting curve determined by DSC analysis. The metallocenes are then combined depending on the desired melting range with respect to melting range maximum and melting range width.
- 15 Taking into account the polymerization activities, computer simulation of the combined DSC curves makes it possible to adjust each desired melting curve type via the type of metallocenes and via the mixing ratio of the metallocenes with one another.
- 20 The number of metallocenes I to be used according to the invention in the polymerization is preferably 2 or 3, in particular 2. However, it is also possible to employ a larger number (such as, for example, 4 or 5) in any desired combination.

Taking into account the polymerization activities and molecular weights at various polymerization temperatures, in the presence of hydrogen as molecular weight regulator or in the presence of comonomers, the computer simulation
5 model can be further refined and the applicability of the process according to the invention further improved.

The cocatalyst used is an aluminoxane of the formula II and/or III, in which n is an integer from 0 to 50, preferably from 10 to 35.

10 The radicals R are preferably identical and are methyl, isobutyl, phenyl or benzyl, particularly preferably methyl.

If the radicals R are different, they are preferably methyl and hydrogen or alternatively methyl and isobutyl,
15 where hydrogen or isobutyl is preferably present to the extent of 0.01 - 40% (number of radicals R). Instead of the aluminoxane, the cocatalyst used in the polymerization can be a mixture comprising the aluminoxane and AlR_3 , where R is as defined above.

20 The aluminoxane can be prepared in various ways by known processes. One of the methods is, for example, to react an aluminum hydrocarbon compound and/or a hydridoaluminum hydrocarbon compound with water (in gas, solid, liquid or bonded form, for example as water of crystallization) in
25 an inert solvent (such as, for example, toluene). In order to prepare an aluminoxane containing different alkyl groups R, two different trialkylaluminum compounds ($AlR_3 + AlR'_3$) in accordance with the desired composition are reacted with water (cf. S. Pasynkiewicz, Polyhedron
30 9 (1990) 429 and EP-A 302 424).

The precise structure of the aluminoxanes II and III is unknown.

Depending on the type of preparation, all aluminoxane

solutions have in common a varying content of unreacted aluminum starting compound, which is in free form or as an adduct.

5 It is possible to preactivate the metallocenes before use in the polymerization reaction, in each case separately or together as a mixture with an aluminoxane of the formula (II) and/or (III). This significantly increases the polymerization activity and improves the grain morphology.

10 The preactivation of the metallocenes is carried out in solution. The metallocenes are preferably dissolved, as a solid, in a solution of the aluminoxane in an inert hydrocarbon. Suitable inert hydrocarbons are aliphatic and aromatic hydrocarbons. Preference is given to toluene
15 or a C_6-C_{10} -hydrocarbon.

The concentration of the aluminoxane in the solution is in the range from about 1% by weight to the saturation limit, preferably from 5 to 30% by weight, in each case based on the total solution. The metallocenes can be
20 employed in the same concentration, but are preferably employed in an amount of from 10^{-4} to 1 mol per mol of aluminoxane. The preactivation time is from 5 minutes to 60 hours, preferably from 5 to 60 minutes. The temperature is from -78 to 100°C , preferably from 0 to 70°C .

25 The metallocenes can also be prepolymerized or applied to a support. For prepolymerization, the (or one of the) olefin(s) employed in the polymerization is preferably used.

30 Examples of suitable supports are silica gels, aluminum oxides, solid aluminoxane, combinations of aluminoxane on a support, such as, for example, silica gel or other inorganic support materials. Another suitable support material is a polyolefin powder in finely divided form.

A further possible embodiment of the process according to the invention comprises using a salt-like compound of the formula $R_xNH_{4-x}BR'$, or of the formula R_3PHBR' , as cocatalyst in place of or in addition to an aluminoxane. In these
5 formulae, x is 1, 2 or 3, R is identical or different and is alkyl or aryl, and R' is aryl, which may also be fluorinated or partly fluorinated. In this case, the catalyst comprises the product of the reaction of the metallocenes with one of said compounds (cf.
10 EP-A 277 004).

In order to remove catalyst poisons present in the olefin, purification by means of an alkylaluminum compound, for example $AlMe_3$ or $AlEt_3$, is advantageous. This
15 purification can be carried out either in the polymerization system itself, or the olefin is brought into contact with the Al compound before addition to the polymerization system and subsequently removed again.

The polymerization or copolymerization is carried out in a known manner in solution, in suspension or in the gas
20 phase, continuously or batchwise, in one or more steps, at a temperature of from -60 to 200°C, preferably from 20 to 80°C. Olefins of the formula $R^a-CH=CH-R^b$ are polymerized or copolymerized. In this formula, R^a and R^b are identical or different and are a hydrogen atom or an
25 alkyl radical having 1 to 14 carbon atoms. However, R^a and R^b may also form a ring together with the carbon atoms connecting them. Examples of such olefins are ethylene, propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-octene, norbornene and norbornadiene. In
30 particular, propylene and ethylene are polymerized.

If necessary, hydrogen is added as molecular weight regulator.

The total pressure in the polymerization system is from 0.5 to 100 bar. The polymerization is preferably carried
35 out in the industrially particularly relevant pressure

range of from 5 to 64 bar.

5 The metallocenes are used in a concentration, based on the transition metal, of from 10^{-3} to 10^{-8} mol, preferably from 10^{-4} to 10^{-7} mol, of transition metal per dm^3 of solvent or per dm^3 of reactor volume. The aluminoxane or the aluminoxane/ AlR_3 mixture is used in a concentration of from 10^{-5} to 10^{-1} mol, preferably from 10^{-4} to 10^{-2} mol, per dm^3 of solvent or per dm^3 of reactor volume. In principle, however, higher concentrations are also possible.

15 If the polymerization is carried out as a suspension or solution polymerization, an inert solvent which is customary for the Ziegler low-pressure process is used. For example, the polymerization is carried out in an aliphatic or cycloaliphatic hydrocarbon, examples which may be mentioned being butane, pentane, hexane, heptane, decane, isooctane, cyclohexane and methylcyclohexane.

20 It is furthermore possible to use a benzine or hydrogenated diesel oil fraction. Toluene can also be used. The polymerization is preferably carried out in the liquid monomer.

If inert solvents are used, the monomers are metered in as gases or liquids.

25 The polymerization can have any desired duration, since the catalyst system to be used according to the invention exhibits only a slight time-dependent drop in polymerization activity.

30 The process according to the invention is distinguished by the fact that the metallocenes described give polymers having a broad, bimodal or multimodal melting range in the industrially relevant temperature range of between 20 and 80°C and with high polymerization activity.

The polyolefin molding compositions according to the invention are particularly suitable for the production of moldings by thermoforming, blow molding, extrusion, injection stretch blow molding and for certain film applications, such as heat-sealing or stretching.

The examples below serve to illustrate the invention in greater detail.

The following abbreviations are used:

- VI = viscosity index in cm^3/g
- 10 M_v = weight average molecular weight in g/mol } determined by gel permeation chromatography
- M_w/M_n = molecular weight dispersity
- 15 MFI (230/5) = melt flow index, measured according to DIN 53735, at a melt temperature of 230°C and with a weight of 5 kg.

Melting points, peak widths, melting ranges and crystallization temperatures were determined by DSC spectrometry (heating/cooling rate $20^\circ\text{C}/\text{min}$).

Example 1

- 20 In each case 5 kg of two different polypropylene powders were mixed, stabilized against chemical degradation under extrusion conditions by means of 20 g of pentaerythrityl tetrakis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate], extruded in a ZSK 28 twin-screw extruder (Werner und
- 25 Pfleiderer) and subsequently granulated. The temperatures in the heating zones were 150°C (feed), 210°C , 250°C , 280°C and 215°C (die plate), the material temperature in the extruder was 275°C , and the extruder screws rotated at 250 rpm. The base polymers used for the mixture had
- 30 the following properties:

Polymer 1: VI = $255 \text{ cm}^3/\text{g}$; MFI (230/5) = 6.8 dg/min ; M_v = $310,000 \text{ g/mol}$; M_w/M_n = 2.2; melting point (melting peak

maximum) 139°C, half-intensity width of the melting peak 5°C, width at quarter peak height 16°C; crystallization point 101°C, half-intensity width of the crystallization peak 4.0°C, width at quarter peak height 5.5°C.

- 5 Polymer 2: VI = 235 cm³/g; MFI (230/5) = 10 dg/min; M_w = 277,000 g/mol; M_w/M_n = 2.3; melting point (melting peak maximum) 152°C, half-intensity width of the melting peak 8°C, width at quarter peak height 12°C; crystallization point 105°C, half-intensity width of the crystallization peak 6°C, width at quarter peak height 7.5°C.
- 10

The novel molding composition prepared by extrusion had the following data:

- VI = 257 cm³/g; MFI (230/5) = 8.7 dg/min; M_w = 300,000 g/mol; M_w/M_n = 2.8; melting range maximum at 150°C, shoulder at 130°C; half-intensity width of the melting peak 19°C, width at quarter peak height 31°C; crystallization peak maximum 105°C; half-intensity width of crystallization peak 8.5°C, width at quarter peak height 11.5°C.
- 15

20 Example 2

Example 1 was repeated, but two other polypropylene components were used and the extruder parameters were 130°C (feed), 155°C, 200°C, 250°C and 250°C (die plate), material temperature 225°C, extruder screw speed 300 rpm.

- 25 Polymer 1: VI = 155 cm³/g; MFI (230/5) = 65 dg/min; M_w = 172,000 g/mol; M_w/M_n = 2.8; melting point (melting peak maximum) 137°C, half-intensity width of the melting peak 10°C, width at quarter peak height 17°C; crystallization point 104°C, half-intensity width of the crystallization peak 5°C, width at quarter peak height 7.5°C.
- 30

Polymer 2: VI = 156 cm³/g; MFI (230/5) = 68 dg/min; M_w = 153,500 g/mol; M_w/M_n = 2.1; melting point (melting peak

maximum) 153°C, half-intensity width of the melting peak 7.5°C, width at quarter peak height 18.8°C; crystallization point 110°C, half-intensity width of the crystallization peak 5°C, width at quarter peak height 7.5°C.

5 Novel molding composition prepared therefrom:

VI = 158 cm³/g; MFI (230/5) = 67 dg/min; M_w = 168,000 g/mol; M_w/M_n = 2.6; melting range maximum at 148°C, shoulder at 138°C; half-intensity width 19°C, width at quarter peak height 31°C; crystallization peak maximum 112°C; half-intensity width of crystallization peak 6°C, width at quarter peak height 10.5°C.

Example 3

Example 1 was repeated, but two other polypropylene components were used and the extruder parameters were 150°C (feed), 160°C, 240°C, 240°C and 240°C (die plate), material temperature 250°C, extruder screw speed 220 rpm.

Polymer 1: VI = 407 cm³/g; MFI (230/5) = 1.9 dg/min; M_w = 488,000 g/mol; M_w/M_n = 2.2; melting point (melting peak maximum) 158°C, half-intensity width of the melting peak 8°C, width at quarter peak height 15°C; crystallization point 109°C, half-intensity width of the crystallization peak 6.5°C, width at quarter peak height 9.5°C.

Polymer 2: VI = 132 cm³/g; MFI (230/5) = 93 dg/min; melting point (melting peak maximum) 138°C, half-intensity width of the melting peak 7°C, width at quarter peak height 18°C; crystallization peak (maximum) 99°C, half-intensity width of the crystallization peak 6.5°C, width at quarter peak height 8°C.

Novel molding composition prepared therefrom:

VI = 247 cm³/g; MFI (230/5) = 12.3 dg/min; M_w = 268,000 g/mol; M_w/M_n = 3.0; melting range maximum at 154°C, shoulder at 141°C; half-intensity width 15°C,

width at quarter peak height 29°C; crystallization at 114°C.

Example 4

5 Example 3 was repeated, but the polymer component 2 used therein was replaced by a polypropylene having the following data:

VI = 353 cm³/g; MFI (230/5) = 2.1 dg/min;
M_w = 465,500 g/mol; M_w/M_n = 2.1; melting point (melting
10 peak maximum) 153°C, half-intensity width of the melting peak 9.5°C, width at quarter peak height 13.5°C; crystallization point 110°C, half-intensity width of the crystallization peak 7.5°C, width at quarter peak height 9°C.

Novel molding composition prepared therefrom:

15 VI = 366 cm³/g; MFI (230/5) = 1.9 dg/min;
M_w = 486,500 g/mol; M_w/M_n = 2.1; double melting range maximum at 157 and 159°C, half-intensity width 17.5°C, width at quarter peak height 29°C; crystallization at 115°C, width at quarter peak height 11°C.

20 Example 5

The procedure was as in Example 1, but 5 kg of polymer 1 from Example 3 and 10 kg of polymer 1 from Example 1 were used. The extruder parameters were 150°C (feed), 160°C, 250°C, 250°C and 240°C (die plate), material temperature
25 255°C, extruder screw speed 190 rpm.

The novel molding composition prepared from these two polymer components had the following data:

VI = 302 cm³/g; MFI (230/5) = 4.2 dg/min;
M_w = 366,500 g/mol; M_w/M_n = 2.5; melting range maximum
30 151°C, half-intensity width 18°C, width at quarter peak height 34.5°C, crystallization at 106°C with a signal half-intensity width of 7.5°C and a width at quarter peak

height of 10.5°C.

Example 6

5 A dry 150 dm³ reactor was flushed with propylene and charged at 20°C with 80 dm³ of a benzine fraction having the boiling range 100-120°C from which the aromatic components had been removed, 50 dm³ of liquid propylene and 150 cm³ of a toluene solution of methylaluminumoxane (corresponding to 250 mmol of Al, molecular weight according to hygroscopic determination 1050 g/mol). The temperature was then adjusted to 40°C. A hydrogen content of 0.05% by volume was set in the gas phase (the content was kept constant during the polymerization by continual topping up of hydrogen). 7.5 mg of a rac-Me₂Si(2-methyl-1-indenyl)₂ZrCl₂ and 45 mg of a rac-Me₂Si(indenyl)₂HfCl₂ were mixed, and the solid was dissolved in 25 cm³ of a toluene solution of methylaluminumoxane (42 mmol of Al) and introduced into the reactor after 15 minutes. The polymerization system was kept at 43°C for 24 hours by cooling. Polymerization was terminated by addition of 2.5 bar of CO₂ gas and the polymer formed (22.6 kg) was separated from the suspension medium in a pressure filter. The product was dried for 24 hours at 80°C/200 mbar. 50 g of pentaerythrityl tetrakis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate] were added to the polymer powder to prevent chemical degradation, and the mixture was extruded in a ZSK 28 twin-screw extruder (Werner und Pfleiderer) and then granulated. The temperatures in the heating zones were 150°C (feed), 200°C, 240°C, 250°C (die plate), the extruder screw speed was 200 rpm, and the material temperature was 250°C.

The novel molding composition had the following data:

VI = 285 cm³/g; MFI (230/5) = 5.4 dg/min;
M_w = 334,500 g/mol; M_w/M_n = 2.2; melting range maximum at 152°C, shoulder at 132°C, half-intensity width of the melting peak 17.5°C, width at quarter peak height 35°C;
35 crystallization peak maximum 106°C; half-intensity width

of crystallization peak 8.5°C; width at quarter peak height 12.5°C.

Example 7

Example 6 was repeated, but the metallocenes used were
5 7.5 mg of phenyl(methyl)Si(2-methyl-1-indenyl)₂ZrCl₂ and
2.5 mg of Me₂Si(2-methyl-4-phenyl-1-indenyl)₂ZrCl₂, the
polymerization temperature was 48°C and a hydrogen
content of 2.5% by volume was set in the gas phase.
21.5 kg of polymer were obtained. The molding composition
10 obtained after extrusion and granulation had the follow-
ing properties:
VI = 194 cm³/g; MFI (230/5) = 28.8 dg/min;
M_w = 238,000 g/mol; M_w/M_n = 2.8; melting range maximum at
157°C, half-intensity width 13.5°C, width at quarter peak
15 height 24°C; crystallization peak maximum 115°C; half-
intensity width 6.5°C; width at quarter peak height
9.5°C.

The molding composition was separated into two consti-
tuents semi-quantitatively by fractional crystallization.

20 Polymer 1 made up about 45% by weight and had the follow-
ing data:
VI = 179 cm³/g; MFI (230/5) = 34 dg/min;
M_w = 195,000 g/mol; M_w/M_n = 2.1; melting point (melting
peak maximum) 151°C, half-intensity width 8.5°C, crystal-
25 lization peak 111°C; half-intensity width 4°C.

Polymer 2 made up about 55% by weight and had the follow-
ing data:
VI = 207 cm³/g; MFI (230/5) = 27 dg/min;
M_w = 259,000 g/mol; M_w/M_n = 2.5; melting point (melting
30 peak maximum) 159°C, half-intensity width 5°C, width at
quarter peak height 12.5°C; crystallization peak at
117°C; half-intensity width 2.5°C and width at quarter
peak height 5°C.

Example 8

Example 6 was repeated, but the polymerization temperature was 50°C, the hydrogen content in the gas space was 2.5% by volume and the metallocenes used were 2.5 mg of
5 $\text{Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$ and 95 mg of $\text{phenyl(methyl)silyl(indenyl)}_2\text{HfCl}_2$. 18.5 kg of polymer were obtained. The extruded molding composition had the following data:

VI = 166 cm^3/g ; MFI (230/5) = 45.8 dg/min;
10 $M_w = 232,000 \text{ g/mol}$; $M_w/M_n = 3.3$; melting range maximum at 156°C, shoulder at 140°C, half-intensity width 13°C, width at quarter peak height 30°C; crystallization peak maximum 115°C, width at quarter peak height 8°C.

The molding composition was separated into two constituents semi-quantitatively by fractional crystallization.
15

Polymer 1 made up about 60% by weight and had the following properties:

VI = 132 cm^3/g ; MFI (230/5) = 98 dg/min;
20 $M_w = 146,000 \text{ g/mol}$; $M_w/M_n = 2.2$; melting point 137°C, half-intensity width 7.5°C; crystallization peak 99°C; half-intensity width 6.5°C.

Polymer 2 made up about 40% by weight and had the following data:

VI = 227 cm^3/g ; MFI (230/5) = 23 dg/min;
25 $M_w = 265,500 \text{ g/mol}$; $M_w/M_n = 2.0$; melting point 160°C, half-intensity width 5.5°C, width at quarter peak height 6°C; crystallization peak 118°C; half-intensity width 3.5°C, width at quarter peak height 5°C.

Example 9

30 Example 6 was repeated, but the polymerization temperature was 50°C, the hydrogen content of the gas space was 1.2% by volume and the metallocenes used were 7.5 mg of

$\text{Me}_2\text{Si}(2\text{-methyl-1-indenyl})_2\text{ZrCl}_2$ and 80 mg of $\text{Me}_2\text{Si}(\text{indenyl})_2\text{HfCl}_2$. 22.5 kg of polymer were obtained, and the extruded molding composition had the following data:

- 5 VI = 130 cm^3/g ; MFI (230/5) = 110 dg/min;
 $M_w = 142,500 \text{ g/mol}$; $M_w/M_n = 2.0$; melting range maximum 149.5°C, shoulder at 137°C, half-intensity width 15.5°C, width at quarter peak height 27.5°C; crystallization peak maximum 112°C, half-intensity width 7.5°C.
- 10 The molding composition was separated semi-quantitatively into two different constituents in a ratio of about 50:50% by weight by fractional crystallization. Of these, polymer 1 had the following data:
- 15 VI = 130 cm^3/g ; MFI (230/5) = 114 dg/min;
 $M_w = 135,000 \text{ g/mol}$; $M_w/M_n = 1.9$; melting point 151°C, half-intensity width 8.5°C; crystallization peak 109°C, half-intensity width 5.5°C.

Polymer 2 is characterized as follows:

- 20 VI = 136 cm^3/g ; MFI (230/5) = 100 dg/min;
 $M_w = 142,500 \text{ g/mol}$; $M_w/M_n = 2.2$; melting point 135°C, half-intensity width 7°C; crystallization peak 97°C, half-intensity width 6.5°C.

Example 10

- 25 The procedure was as in Example 7, but the ratio between the two metallocenes used was changed from 7.5 mg/2.5 mg to 10.4 mg/1.8 mg.

The molding composition obtained after extrusion had the following properties:

- 30 VI = 192 cm^3/g ; MFI (230/5) = 30.4 dg/min;
 $M_w = 241,500 \text{ g/mol}$; $M_w/M_n = 2.3$; melting range maximum at 155°C, half-intensity width 12°C, width at quarter peak height 22.5°C; crystallization at 113°C.

Example 11

The procedure was as in Example 7, but the ratio between the two metallocenes used was changed from 7.5 mg/2.5 mg to 3.9 mg/5.2 mg.

- 5 The molding composition obtained after extrusion had the following properties:

VI = 197 cm³/g; MFI (230/5) = 28.9 dg/min;
M_w = 214,000 g/mol; M_w/M_n = 2.5; melting range maximum at
158°C, width at quarter peak height 24°C; crystallization
10 at 116°C.

Example 12

The procedure was as in Example 8, but the ratio between the two metallocenes used was changed from 2.5 mg/95 mg to 1.5 mg/125 mg.

- 15 The molding composition examined after extrusion had the following properties:

VI = 162 cm³/g; MFI (230/5) = 62 dg/min;
M_w = 198,000 g/mol; M_w/M_n = 2.7; melting range maximum at
151°C, shoulder at 135°C, half-intensity width 16°C,
20 width at quarter peak height 32.5°C; crystallization at
114°C.

Example 13

The procedure was as in Example 8, but the ratio between the two metallocenes used was changed from 2.5 mg/95 mg
25 to 3.6 mg/51.5 mg.

The molding composition examined after extrusion had the following properties:

VI = 187 cm³/g; MFI (230/5) = 37.1 dg/min;

$M_w = 209,500$ g/mol; $M_w/M_n = 2.9$; melting range maximum at 157°C , width at quarter peak height 27.5°C ; crystallization at 116°C .

Example 14

- 5 A dry 24 dm^3 reactor was flushed with propylene and charged with 10 dm^3 (S.T.P.) of hydrogen, 12 dm^3 of liquid propylene and 32 cm^3 of a toluene solution of methylaluminumoxane (corresponding to 52 mmol of Al, mean degree of oligomerization $n = 21$). The contents were stirred at
10 30°C for 15 minutes at 250 rpm.

- In parallel, 6.2 mg of rac-ethylene(2-methyl-1-indenyl) $_2\text{ZrCl}_2$ and 1.0 mg of rac- Me_2Si (2-methyl-4-phenyl-1-indenyl) $_2\text{ZrCl}_2$ were dissolved in 12 cm^3 of a toluene solution of methylaluminumoxane (20 mmol of Al) and pre-
15 activated by standing for 15 minutes. The solution was introduced into the reactor, and the mixture was polymerized at 60°C for 1 hour. 2.05 kg of polypropylene were obtained. The molding composition prepared by extrusion had the following data:

- 20 VI = $285\text{ cm}^3/\text{g}$; MFI (230/5) = 7.5 dg/min ; $M_w = 395,000$ g/mol; $M_w/M_n = 3.3$; melting range maximum 159°C , shoulder at 151°C , half-intensity width 14°C , width at quarter peak height 30.5°C ; crystallization at 116°C .

25 Example 15

- The procedure was as in Example 14, but no hydrogen was used, the polymerization temperature was 70°C and the metallocenes used were 1.8 mg of rac-ethylidene(2-methyl-4,6-diisopropyl-1-indenyl) $_2\text{ZrCl}_2$ and 2.5 mg of rac-
30 Me_2Si (2-methyl-4,5-benzoindenyl) $_2\text{ZrCl}_2$. 2.07 kg of polymer powder were obtained. The molding composition prepared by extrusion had the following data:

VI = 245 cm³/g; MFI (230/5) = 8.5 dg/min;
M_w = 296,500 g/mol; M_w/M_n = 2.9; melting range maximum
145°C, half-intensity width 16.5°C, width at quarter peak
height 25.5°C; crystallization at 109°C.

5 Example 16

The procedure was as in Example 15, but the metallocenes
used were 5.0 mg of dimethylmethylen (9-fluorenyl)-
(cyclopentadienyl)ZrCl₂ and 5.0 mg of phenyl(methyl)-
methylen (9-fluorenyl) (cyclopentadienyl)ZrCl₂. 1.63 kg of
10 polypropylene were obtained, giving, after extrusion, a
molding composition having the following properties:

VI = 141 cm³/g; MFI (230/5) = 32.5 dg/min;
M_w = 125,500 g/mol; M_w/M_n = 2.5; melting range maximum at
125 and 132°C, half-intensity width 24.5°C, width at
15 quarter peak height 41.5°C; crystallization at 57°C and
75°C, half-intensity width 31.5°C.

Example 17

A dry 24 dm³ reactor was flushed with propylene and
charged with 9.5 dm³ (S.T.P.) of hydrogen and 12 dm³ of
20 liquid propylene. 35 cm³ of a toluene solution of methyl-
aluminoxane (corresponding to 52 mmol of Al, mean degree
of oligomerization n = 20) were then added. In parallel,
6.5 mg of rac-phenyl(methyl)silyl(2-methyl-4,6-diiso-
propyl-1-indenyl)₂ZrCl₂ were dissolved in 13.5 cm³ of a
25 toluene solution of methylaluminoxane (20 mmol of Al) and
preactivated by standing for 5 minutes.

The solution was then introduced into the reactor, and
the mixture was polymerized at 60°C for 1 hour with
continuous addition of 60 g of ethylene. 2.59 kg of
30 random copolymer were obtained. The ethylene content of
the copolymer was 2.0% by weight.

VI = 503 cm³/g; M_w = 384,000 g/mol; M_w/M_n = 2.0; melting

point = 139°C.

A second polymerization was carried out in the same way, but with 5 dm³(S.T.P.) of hydrogen and without addition of ethylene. The metallocene used was 2.5 mg of rac-dimethylsilyl(2-methyl-4-phenyl-1-indenyl)₂ZrCl₂. 1.71 kg of polypropylene were obtained.

VI = 524 cm³/g; $M_w = 448,000$ g/mol; $M_w/M_n = 2.0$; melting point = 162°C.

1.5 kg of each of the polymers obtained in the two polymerization reactions were stabilized against chemical degradation under extrusion conditions by means of 6 g of pentaerythrityl tetrakis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate], extruded in a ZSK 28 twin-screw extruder (Werner und Pfleiderer) and subsequently granulated. The temperatures in the heating zones were 150°C (feed), 250°C, 270°C, 270°C and 270°C (die plate), the material temperature was 285°C and the extruder screws rotated at 150 rpm.

The molding composition prepared in this way had the following properties:

VI = 548 cm³/g; $M_w = 424,000$ g/mol; $M_w/M_n = 2.5$; melting range maximum 158°C, shoulder at 143°C, half-intensity width 19.5°C, width at quarter peak height 35.5°C; crystallization at 119°C, half-intensity width 11.5°C.

Example 18

The procedure was as in Example 14, but the second metallocene used instead of rac-Me₂Si(2-methyl-4-phenyl-1-indenyl)₂ZrCl₂ was the compound Ph(Me)Si(2-methyl-4-phenyl-1-indenyl)₂ZrCl₂.

1.95 kg of polypropylene were obtained. The extruded molding composition had the following data:

VI = 325 cm³/g; MFI (230/5) = 3.9 dg/min; melting range maximum 160°C, shoulder at 150°C, half-intensity width

16°C, width at quarter peak height 31°C; crystallization at 114°C.

Example 19

The procedure was as in Example 14, but the second
5 metallocene used instead of $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$ was the compound $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$. 2.55 kg of polypropylene were obtained. The extruded molding composition had the following data:

10 VI = 419 cm^3/g ; MFI (230/5) = 0.9 dg/min; melting range maximum 162°C, shoulder at 150°C, half-intensity width 18°C, width at quarter peak height 30°C; crystallization at 110°C.

Example 20

15 The procedure was as in Example 14, but the metallocenes used were 4.0 mg of $\text{rac-Me}_2\text{Si}(2,5,6\text{-trimethyl-1-indenyl})_2\text{-ZrCl}_2$ and 0.8 mg of $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$. 2.30 kg of polypropylene were obtained. The extruded molding composition had the following data:
20 VI = 379 cm^3/g ; MFI (230/5) = 3.0 dg/min; melting peak maximum 161°C, shoulder at 137°C, half-intensity width 22°C, width at quarter peak height 35°C; crystallization at 112°C.

Example 21

25 The procedure was as in Example 14, but the metallocenes used were 3.0 mg of $\text{rac-Me}_2\text{Si}(4,5\text{-benzo-1-indenyl})_2\text{ZrCl}_2$ and 0.8 mg of $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-(1-naphthyl)-1-indenyl})_2\text{ZrCl}_2$. 2.10 kg of polypropylene were obtained. The extruded molding composition had the following data:
30 VI = 225 cm^3/g ; MFI (230/5) = 23.5 dg/min; melting peak maximum 161°C, shoulder at 140°C, half-intensity width 17°C, width at quarter peak height 32°C; crystallization at 111°C.

Example 22

The procedure was as in Example 14, but the metallocenes used were 6.0 mg of $\text{rac-Me}_2\text{Si}(4\text{-phenyl-1-indenyl})_2\text{ZrCl}_2$ and 0.8 mg of $\text{rac-Me}_2\text{Si}(2\text{-methyl-4-phenyl-1-indenyl})_2\text{ZrCl}_2$. 2.23 kg of polypropylene were obtained. The extruded molding composition had the following data: VI = 220 cm^3/g ; MFI (230/5) = 25 dg/min; melting peak maximum 160°C, shoulder at 149°C, half-intensity width 15°C, width at quarter peak height 30°C; crystallization at 115°C.

Example 23

The procedure was as in Example 22, but in addition 70 g of ethylene were metered continuously into the reactor during the 1-hour polymerization time. 2.35 kg of ethylene/propylene copolymer were obtained. VI = 190 cm^3/g ; MFI (230/5) = 45 dg/min; melting peak maximum 148°C, shoulder at 132°C, half-intensity width 14°C. The copolymer contained 2.5% by weight of ethylene distributed randomly.

20 Comparative Example 1

The procedure was as in Example 1, but the following polymers were used:

Polymer 1: VI = 230 cm^3/g ; MFI (230/5) = 15 dg/min; $M_w = 268,000$ g/mol; $M_w/M_n = 2.0$; melting point (maximum) 157°C, half-intensity width of the melting peak 7°C; width at quarter peak height 10°C; crystallization point 112°C.

Polymer 2: VI = 235 cm^3/g ; MFI (230/5) = 12 dg/min; $M_w = 272,000$ g/mol; $M_w/M_n = 2.1$; melting point (maximum) 154°C, half-intensity width of the melting peak 8°C; width at quarter peak height 12°C; crystallization point 109°C, width of crystallization peak (at quarter peak

height) 5°C.

Comparative Example 2:

The procedure was as in Example 1, but the following polymers were used:

- 5 Polymer 1: VI = 260 cm³/g; MFI (230/5) = 5 dg/min; M_w = 295,000 g/mol; M_w/M_n = 2.3; melting point (maximum) 149°C, half-intensity width of the melting peak 6°C; width at quarter peak height 13°C; crystallization point 106°C.
- 10 Polymer 2: as polymer 2 in Example 1

The non-novel molding composition prepared by extrusion had the following data:

- VI = 249 cm³/g; MFI (230/5) = 8 dg/min; M_w = 294,500 g/mol; M_w/M_n = 2.6; melting point (maximum) 151°C, half-intensity width of the melting peak 8°C; width at quarter peak height 12°C; crystallization point 105°C.
- 15

Comparative Example 3

- The procedure was as in Example 1, but the following polymers were used:
- 20

Polymer 1: as polymer 1 in Example 1.

- Polymer 2: VI = 230 cm³/g; MFI (230/5) = 14 dg/min; M_w = 274,500 g/mol; M_w/M_n = 2.3; melting point (melting peak maximum) 135°C, half-intensity width of the melting peak 5.5°C; width at quarter peak height 14°C; crystallization point 102°C.
- 25

The non-novel molding composition prepared by extrusion had the following data:

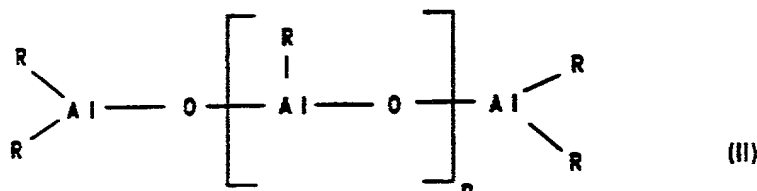
VI = 240 cm³/g; MFI (230/5) = 12 dg/min;
M_w = 287,500 g/mol; M_w/M_n = 2.4; melting point (maximum)
137°C, half-intensity width of the melting peak 5.5°C;
width at quarter peak height 14°C; crystallization point
5 102°C, half-intensity width of the crystallization peak
4°C, width at quarter peak height 5°C.

Claims:

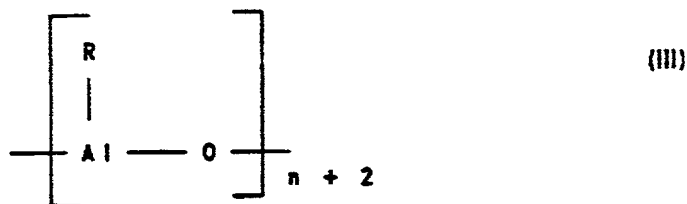
1. A polyolefin molding composition which has a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, the half-intensity width of the melting peak is broader than 10°C and the width determined at quarter peak height is greater than 15°C.
2. A polyolefin molding composition as claimed in claim 1, wherein the half-intensity width of the crystallization peak is greater than 4°C and the width of the crystallization peak determined at quarter peak height is greater than 6°C.
3. A polyolefin molding composition as claimed in claim 1, which additionally contains nucleating agents, stabilizers, antioxidants, UV absorbers, light stabilizers, metal deactivators, free-radical scavengers, fillers and reinforcing agents, compatibilizers, plasticizers, lubricants, emulsifiers, pigments, optical brighteners, flameproofing agents, antistatics or blowing agents.
4. A process for the preparation of a polyolefin molding composition as claimed in claim 1, by mixing at least two polyolefins of different melting points, where the melting points of at least two of the polyolefins must differ by at least 5°C, the viscosity indices are greater than VI = 10 cm³/g and the molecular weights M_n are greater than 5000 g/mol.
5. A process for the preparation of a polyolefin molding composition as claimed in claim 1, by direct polymerization or copolymerization of at least two polyolefins of different melting point, where the melting points must differ by at

least 5°C.

6. The process as claimed in claim 5, wherein the olefins have the formula $R^aCH=CHR^b$, in which R^a and R^b are identical or different and are a hydrogen atom or an alkyl radical having 1 to 14 carbon atoms, or R^a and R^b , together with the atoms connecting them, can form a ring, and are polymerized at a temperature of from -60 to 200°C, and a pressure of from 0.5 to 100 bar, in solution, in suspension or in the gas phase, in the presence of a catalyst, where the catalyst comprises at least two transition-metal components (metallocenes) and an aluminoxane of the formula II



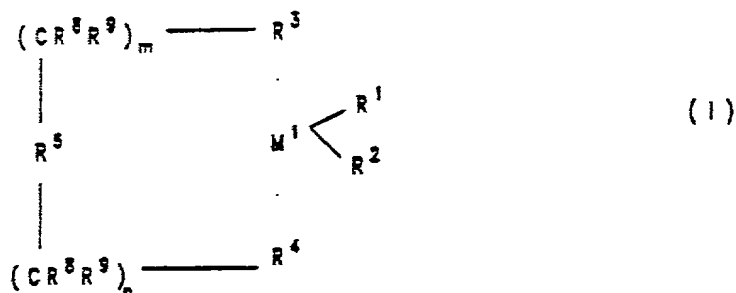
for the linear type and/or of the formula III



- for the cyclic type, where, in the formulae II and III, the radicals R may be identical or different and are a C_1 - C_6 -alkyl group, a C_1 - C_6 -fluoroalkyl group, a C_6 - C_{18} -aryl group, a C_6 - C_{18} -fluoroaryl group or hydrogen, and n is an integer from 0 to 50, and the aluminoxane component may additionally contain a compound of the formula AlR_3 ,

where the transition-metal component used comprises

at least two metallocenes of the formula I:



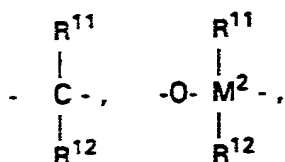
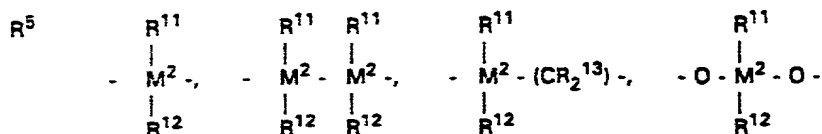
in which

M^1 is Zr, Hf or Ti,

R^1 and R^2 are identical or different and are a hydrogen atom, a C_1 - C_{10} -alkyl group, a C_1 - C_{10} -alkoxy group, a C_6 - C_{10} -aryl group, a C_6 - C_{10} -aryloxy group, a C_2 - C_{10} -alkenyl group, a C_7 - C_{40} -arylalkyl group, a C_7 - C_{40} -alkylaryl group, a C_8 - C_{40} -arylalkenyl group or a halogen atom,

R^3 and R^4 are identical or different and are a monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radical which, together with the metal atom M^1 , can form a sandwich structure,

R^5 is



$=\text{BR}^{11}$, $=\text{AlR}^{11}$, $-\text{Ge}-$, $-\text{Sn}-$, $-\text{O}-$, $-\text{S}-$, $=\text{SO}$, $=\text{SO}_2$, $=\text{NR}^{11}$, $=\text{CO}$,

$=PR^{11}$ or $=P(O)R^{11}$,

where

R^{11} , R^{12} and R^{13} are identical or different and are a hydrogen atom, a halogen atom, a C_1 - C_{10} -alkyl group, a C_1 - C_{10} -fluoroalkyl group, a C_6 - C_{10} -aryl group, a C_6 - C_{10} -fluoroaryl group, a C_1 - C_{10} -alkoxy group, a C_2 - C_{10} -alkenyl group, a C_7 - C_{10} -arylalkyl group, a C_8 - C_{10} -arylalkenyl group or a C_7 - C_{10} -alkylaryl group, or R^{11} and R^{12} or R^{11} and R^{13} , in each case together with the atoms connecting them, form a ring, and M^2 is silicon, germanium or tin, R^8 and R^9 are identical or different and are as defined for R^{11} , m and n are identical or different and are zero, 1 or 2, where m plus n is zero, 1 or 2.

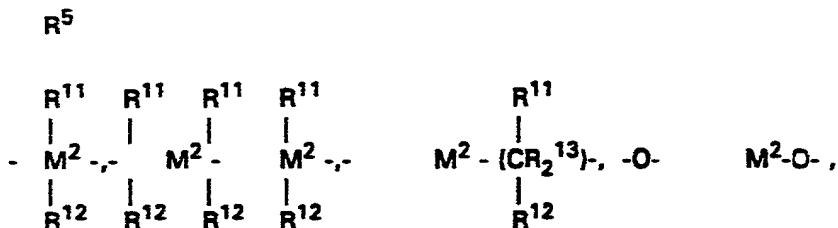
7. The process as claimed in claim 6, wherein

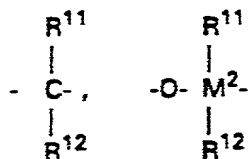
M^1 is Zr or Hf,

R^1 and R^2 are identical or different and are a hydrogen atom, a C_1 - C_3 -alkyl group, a C_1 - C_3 -alkoxy group, a C_6 - C_8 -aryl group, a C_6 - C_8 -arvloxy group, a C_2 - C_4 -alkenyl group, a C_7 - C_{10} -arylalkyl group, a C_7 - C_{12} -alkylaryl group, a C_8 - C_{12} -arylalkenyl group or chlorine,

R^3 and R^4 are identical or different, monocyclic or polycyclic, unsubstituted or substituted hydrocarbon radicals which, together with the metal atom M^1 , can form a sandwich structure,

R^5 is





5
10
=BR¹¹, =AlR¹¹, -Ge-, -Sn-, -O-, -S-, =SO-, =SO₂, =NR¹¹,
=CO, =PR¹¹ or =P(O)R¹¹, where R¹¹, R¹² and R¹³ are
identical or different and are a hydrogen atom, a
halogen atom, a C₁-C₄-alkyl group, CF₃ group, a C₆-C₈-
aryl group, a pentafluorophenyl group, a C₁-C₄-alkoxy
group, a C₂-C₄-alkenyl group, a C₇-C₁₀-arylalkyl
group, a C₆-C₁₂-arylalkenyl group or a C₇-C₁₂-alkyl-
aryl group, or R¹¹ and R¹² or R¹¹ and R¹³, in each case
together with the atoms connecting them, form a
ring,

M² is silicon or germanium,
R⁶ and R⁹ are identical or different and are as
defined for R¹¹,
m and n are identical or different and are zero or
15
1, where m plus n are zero or 1.

8. The process as claimed in claim 6, wherein
M² is zirconium or hafnium, R¹ and R² are identical
and are methyl or chlorine,
R⁴ and R³ are indenyl, cyclopentadienyl or fluorenyl,
20
where these ligands may carry additional substi-
tuents as defined for R¹¹, R¹² and R¹³, where the
substituents may be different and, with the atoms
connecting them, may also form rings,
R⁵ is a



radical, and n plus m are zero or 1.

9. The method of using a molding composition as claimed in

claim 1 for the production of
moldings.

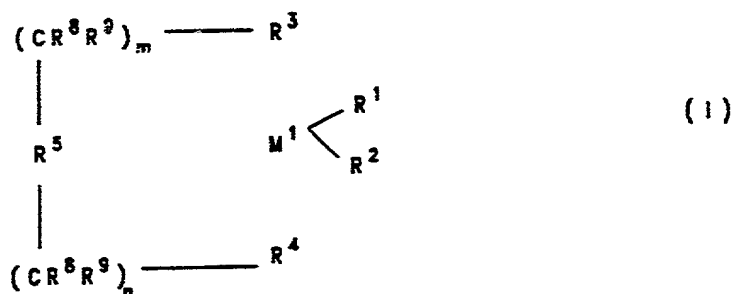
10. A molding which can be produced from a molding
composition as claimed in claim 1.

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Abstract of the disclosure

Polyolefin molding composition having a broad melting range, process for its preparation, and its use

- 5 Polyolefin molding compositions which have a broad, bimodal or multimodal melting range in the DSC spectrum, where the melting range maximum is between 120 and 165°C, are obtained by polymerization or copolymerization of at least two olefins to give polyolefins of different melting point. The olefins have the formula $R^aCH=CHR^b$, and
 10 the catalyst system comprises an aluminoxane and at least two transition-metal components of the formula I



in which

M^1 is Zr, Hf or Ti.